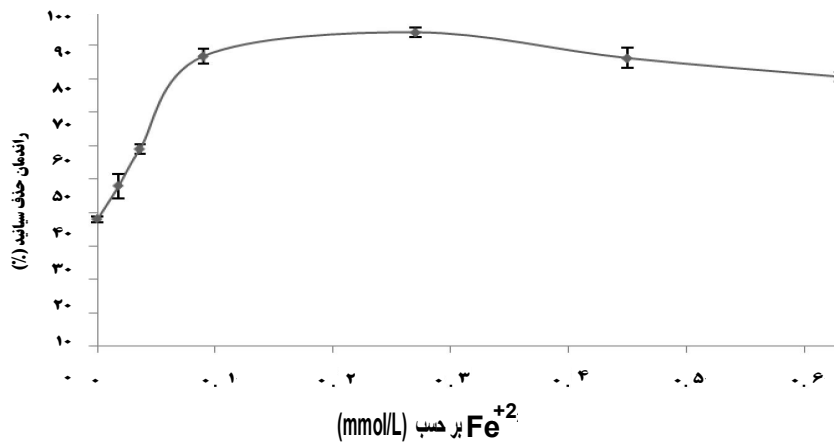
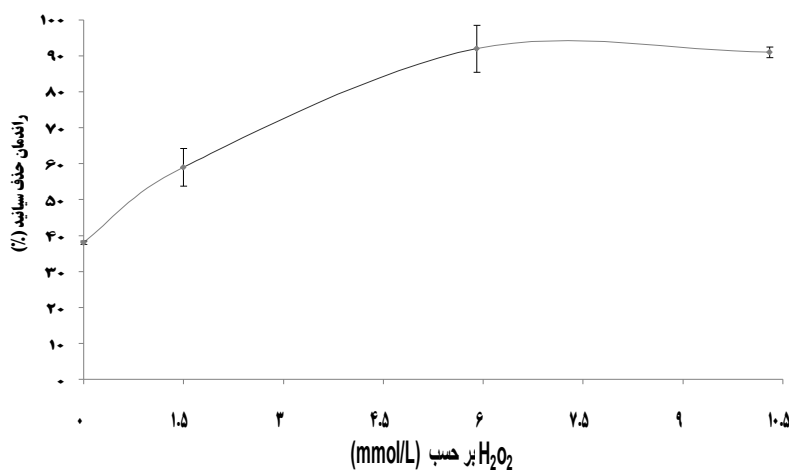


$Fe^{2+} = \frac{A}{\epsilon \cdot d \cdot c}$ mmol/L) $Fe^{2+} / H_2O_2 = \frac{A}{\epsilon \cdot d \cdot c}$
 ppm
 pH
 / - /
 " ()
 Fe^{2+} : one factor at a time
 mmol H_2O_2 ; $\frac{A}{\epsilon \cdot d \cdot c}$ - $\frac{A}{\epsilon \cdot d \cdot c}$ mmol
 " $\frac{A}{\epsilon \cdot d \cdot c}$ - $\frac{A}{\epsilon \cdot d \cdot c}$ mmol
 " $\frac{A}{\epsilon \cdot d \cdot c}$ - $\frac{A}{\epsilon \cdot d \cdot c}$ mmol
 (CECIL-model 7100) vis-uv
 " $\frac{A}{\epsilon \cdot d \cdot c}$ nm
 " $\frac{A}{\epsilon \cdot d \cdot c}$
 4500-E - CN
 ($\frac{A}{\epsilon \cdot d \cdot c}$)
 " Merck
 " Excel
 " Fe^{2+} / H_2O_2 pH
 " pH
 " $\frac{A}{\epsilon \cdot d \cdot c}$ mg/L
 $\frac{A}{\epsilon \cdot d \cdot c}$ mg/L " $\frac{A}{\epsilon \cdot d \cdot c}$ mmol/L
 " / L
 L " $\frac{A}{\epsilon \cdot d \cdot c}$ mmol
 pH pH " " N
 pH= " ! $\frac{A}{\epsilon \cdot d \cdot c}$ N

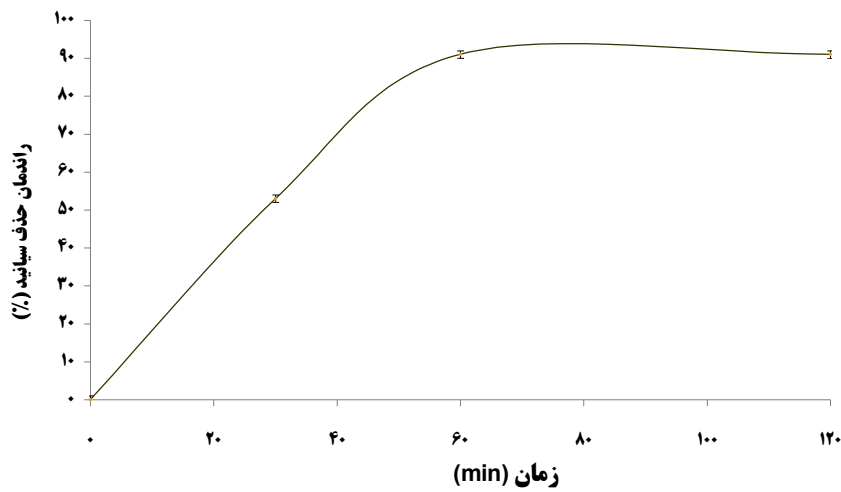


($\text{H}_2\text{O}_2 = 1 \text{ mmol/L}$ | $\text{pH} = 5$ | $\text{Fe}^{2+} = 1 \text{ mmol}$)

در این مطالعه، درصد حذف یون Fe^{2+} با تغییر غلظت آن در محلول، در حالی که غلظت H_2O_2 و pH ثابت نگه داشته شد، بررسی شد. نتایج نشان داد که درصد حذف با افزایش غلظت Fe^{2+} تا حدی افزایش می‌یابد و سپس کمی کاهش می‌یابد. این رفتار می‌تواند به دلیل تغییر در دینامیک واکنش یا تغییر در شرایط تعادل باشد. همچنین، در این شرایط، درصد حذف در محدوده 45 تا 95 درصد متغیر بود.



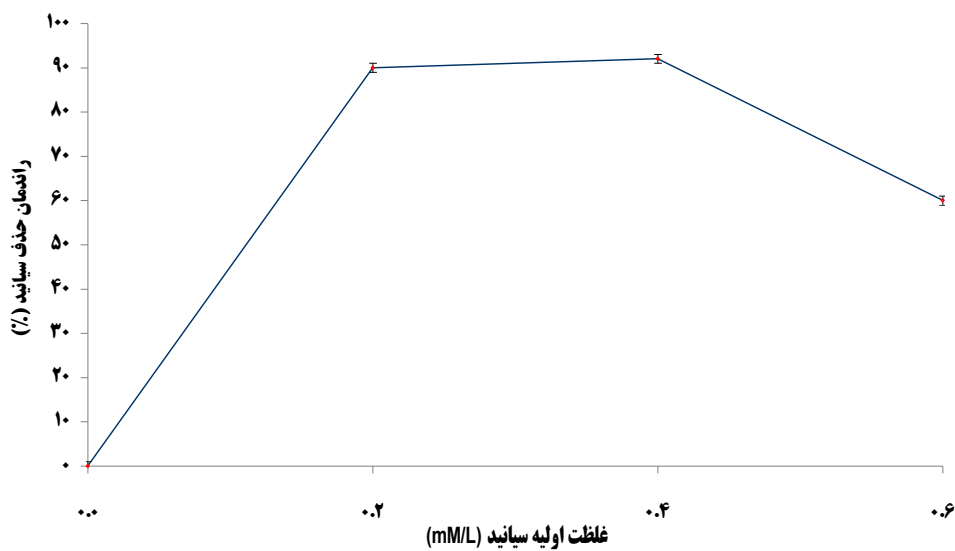
($\text{Fe}^{2+} = 1 \text{ mM/L}$ | $\text{pH} = 5$ | $\text{Fe}^{2+} = 1 \text{ mmol}$)



($\text{Fe}^{2+} = 0.2 \text{ mmol/L}$, $\text{H}_2\text{O}_2 = 0.2 \text{ mmol/L}$, $\text{pH} = 3$)

($\text{Fe}^{2+} = 0.2 \text{ mmol/L}$, $\text{H}_2\text{O}_2 = 0.2 \text{ mmol/L}$, $\text{pH} = 3$)

در این آزمایش، pH را در محدوده 3 تا 11 تغییر دادیم. نتایج نشان داد که در pH 3، راندمان حذف سیانید بیشترین مقدار را دارد. این امر به دلیل تشکیل گونه های فعال تر در این pH است. همچنین، در pH 11، راندمان حذف سیانید به شدت کاهش می یابد. بنابراین، pH 3 بهترین شرایط برای حذف سیانید است.



($\text{Fe}^{2+} = 0.2 \text{ mmol/L}$, $\text{H}_2\text{O}_2 = 0.2 \text{ mmol/L}$, $\text{pH} = 3$)

($\text{Fe}^{2+} = 0.2 \text{ mmol/L}$, $\text{H}_2\text{O}_2 = 0.2 \text{ mmol/L}$, $\text{pH} = 3$)

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$$Fe^{2+}/H_2O_2 <$$

i ymin

ñ y

yy

Lipczynska

fl)

Kavitha

y/ mmol

fl

L

(L

ymin

H₂O₂

ç/

ñ ç ðé ç/ mM

H₂O₂:CN

mmol/L

(H₂O₂:CN) =

è mg/L

çmin

(Fe²⁺L

y/

Masahafi

(H₂O₂:CN) =

mg/L

èçmin

éç mg/L

(é L

$$= y/ \text{ mmol/L } \text{pH} = \text{ ç/ mmol/L}$$

$$Fe^{2+}/H_2O_2 = y/y \text{) } H_2O_2 = / \text{ mmol/L } iFe^{2+}$$

ñ çmin

ç/ mmol

ñ ç ðé ç/

$$Fe^{2+} \text{ pH} = \text{ L pH}$$

fl L

pH

(L

Fe²⁺

pH

OH⁰ H⁺

H₂O₂

fl L

OH⁰

$$Fe^{2+}/H_2O_2 = y/y$$

H₂O₂

Fe²⁺

(L



Ly/y

Fe²⁺/H₂O₂

(L



Fe²⁺/H₂O₂ <

Neyens

y/ mmolL

fl L

y/ mmol

$$Fe^{2+}/H_2O_2 = y/ / \text{ mmol/L}$$

y/y

H₂O₂

(L



Fe²⁺/H₂O₂

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The Study of Fenton Performance in Removal of Cyanide from Aqueous Solution

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ABSTRACT

Background and Objectives: Cyanide is a toxic pollutant existing in the various industrial effluents such as iron and steel, coal mining, non-ferrous metals manufacturing and metal plating. Its presence in water resources and wastewater, as serious hazardous substances leads to undesirable effects on both the environment and human. Thus, its concentration control is essential for human health. The main goal of this study was to evaluate Fenton process efficiency in cyanide removal from aqueous solution.

Materials and Methods: This is an experimental study Conducted at Lab scale in a batch system. We investigated effect of different variables including; pH, mole ratio of $\text{Fe}^{2+}/\text{H}_2\text{O}_2$, contact time, and initial concentration of cyanide. Data were analyzed using Excel software.

Results: We found that cyanide with initial concentrations of 0.4 mM/L was reduced by 92 %. This removal result was related to oxidizing agent of hydroxyl radicals under optimum conditions including; pH = 4, molar ratio $\text{Fe}^{2+}/\text{H}_2\text{O}_2 = 0.046$ ($\text{Fe}^{2+} = 0.27$ mM/L) after 60 min reaction time. An increase in reaction time was not improved cyanide removal efficiency. Moreover, the Fenton process efficiency in cyanide removal decreased from 92 to 60 %, by increasing the initial cyanide concentration from 0.4 to 0.6 mM/L.

Conclusion: It can be concluded that Fenton oxidation Process can be considered as a suitable alternative for cyanide removal to achieve environmental standards.

Keywords: Advanced oxidation, Hydrogen peroxide, Fenton, Wastewater treatment, Cyanide

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